

# Green Hydrogen Production: Mitigation Measures against Explosions

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# Contents

- “Dilution Ventilation” as a mitigation measure against internal explosions
  - Literature on ventilation
  - Experimental data for hydrogen
- Modelling and validation
- Modelling as a design support
- Conclusions

# Dilution Ventilation

# Introduction

- Green Hydrogen Production often makes uses of enclosures
- *Dilution ventilation* to prevent build-up of flammable gas
- Minimize recirculation and stagnant regions
- Considerable research and industry guidance
- Quantitative frameworks to evaluate performance
- Role for modelling tools (and *in-situ* measurements)
- Mostly based on natural gas
- Need to account for hydrogen and its increased reactivity
- Modelling tools also need to be tested for hydrogen



# Objectives

- Literature on ventilation (*performance-based approach*)
- Hydrogen-specific literature on ventilation
- Test an engineering CFD tool on hydrogen data
- Demonstrate use of the model to support design

# Dilution Ventilation (natural gas)

- Large (“catastrophic”) releases cannot be mitigated with dilution ventilation that is meant to protect from Small leaks
- ACH is not a suitable parameter to evaluate the effectiveness of the ventilation
- A measure of the flammable volume is more adequate
- The flammable volume correlates with the ratio “release rate/ ventilation rate” (and not with ACH)
- To evaluate ventilation, we need to define a release rate first! (0.25m<sup>2</sup> to 25mm<sup>2</sup>)
- The research has produced the ISO-21789 standard (for GTs)
- The flammable volume generated by the leak should be less than 0.1% of the enclosure volume
- The performance of ventilation needs to be demonstrated with CFD and measurements
- This criterion has been tested for enclosures of 100m<sup>3</sup> and if  $V_f < 0.1\%$ ,  $P_{max} < 10\text{mbarg}$
- CFD performed well when compared to experiments where the wind conditions were “steady” but less well for highly unsteady wind conditions
- For large enclosures (>1,000m<sup>3</sup>) ventilation needs to be complemented with enhancing Gas Detection
- Ventilation rate is not the only parameter to design for: the distribution of air-inlets and outlets is also key

# Guidance (general)

- API RP 505 – 2025 Edition (January 2025)
- EI 15 (2024)
- IEC 60079 – 10-1 (2020)
- ISO 21789:2022 (GTs, natural gas!)

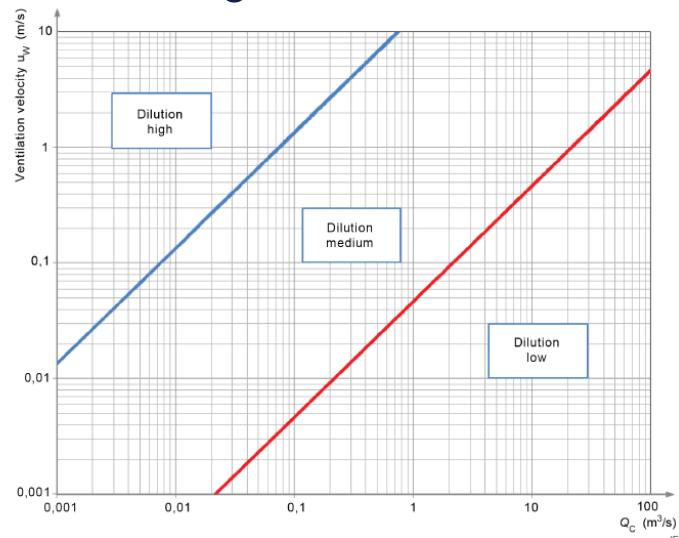
## IEC: Ventilation Criterion

### hole size (1-2 mm)

Table B.1 – Suggested hole cross sections for secondary grade of releases

Type of item	Item	Leak Considerations		
		Typical values for the conditions at which the release opening will not expand		Typical values for the conditions at which the release opening may expand, e.g. erosion
		$S$ (mm $^2$ )	$S$ (mm $^2$ )	$S$ (mm $^2$ )
Sealing elements on fixed parts	Flanges with compressed fibre gasket or similar	$\geq 0,025$ up to 0,25	$> 0,25$ up to 2,5	(sector between two bolts) $\times$ (gasket thickness) usually $\geq 1$ mm
	Flanges with spiral wound gasket or similar	0,025	0,25	(sector between two bolts) $\times$ (gasket thickness) usually $\geq 0,5$ mm
	Ring type joint connections	0,1	0,25	0,5
	Small bore connections up to 50 mm $^3$	$\geq 0,025$ up to 0,1	$> 0,1$ up to 0,25	1,0
Sealing elements on moving parts at low speed	Valve stem packings	0,25	2,5	To be defined according to Equipment Manufacturer's Data but not less than 2,5 mm $^2$
	Pressure relief valves <sup>b</sup>	0,1 $\times$ (orifice section)	NA	NA
Sealing elements on moving parts at high speed	Pumps and compressors <sup>c</sup>	NA	$\geq 1$ up to 5	To be defined according to Equipment Manufacturer's Data and the Unit Configuration but not less than 5 mm $^2$

### “degree of dilution”



ISO

INTERNATIONAL  
STANDARD

ISO  
21789

Second edition  
2022-07

Gas turbine applications — Safety

Applications des turbines à gaz — Sécurité

# Dilution Ventilation Research (hydrogen)

- Releases in non-ventilated enclosures. A characteristic stratification (in the vertical direction) with almost homogeneous concentration near the ceiling (InsHyde, HySea, Hy4Heat)
- Releases in naturally ventilated enclosures. Natural ventilation can be buoyancy-driven, wind-driven or a combination of both. Depending on speed and direction, wind can either “assist” or “oppose” the buoyancy. Recirculation regions can also disrupt the buoyancy-driven ventilation. Configurations with multiple vents at multiple locations of the enclosure are more effective (HSE UK, tests, HyIndoor)
- Releases in forced ventilated enclosures. Very few data, conflicting findings if not properly analysed

Author	Volume (m <sup>3</sup> )	R (hydrogen/ventilation rate)	Effect (conc.)
Ekoto &al., 2012	45	3.5x10 <sup>-1</sup>	none
Lach &al., 2021	60	1.1x10 <sup>-2</sup>	modest
Kim & Hwang, 2024	1.3	8.7x10 <sup>-4</sup>	considerable

# Guidance (hydrogen)

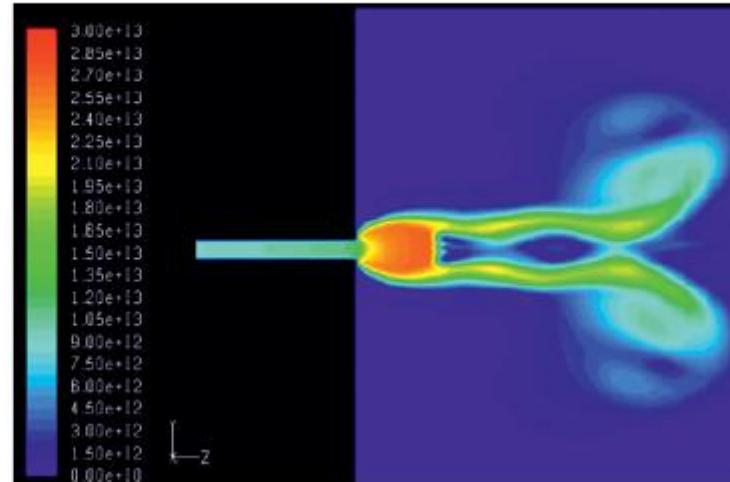
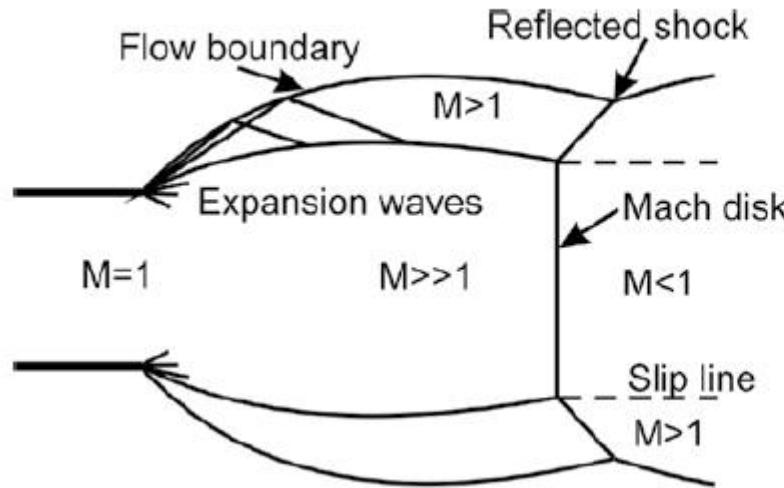
- NFPA 2: Hydrogen Technologies Code: “*ventilation should be at a rate not less than 0.3 Nm<sup>3</sup>/min/m<sup>2</sup> of floor area...*”
- ISO/TR 15916: Basic Considerations for the Safety of Hydrogen Systems: “*Ventilation system should remove hydrogen from the confined space or at least keep its concentration below the appropriate lower flammability limit*”
- DNV-ST-J301: Electrolyser Systems: “*The level of dilution shall be sufficient to reduce the concentration of hydrogen to no greater than 1%, i.e. equivalent to 25% of the lower explosive limit*”.

# Model Validation/Testing

# Model Validation/Testing (FLACS)

- Source term (release rate, velocity, temperature, expanded diameter)
- Free jet structure (under-expanded jet)
- Dispersion in the enclosures (ventilation, obstacles, confinement, etc.)

# Source term



Several approaches:

- Birch et al., 1984
- Ewan & Modie, 1986
- Schefer et al., 2007
- Molkov et al., 2009

- Sonic velocity at the “notional nozzle” exit seems to work better
- Birch (subsonic) also OK (tends to overestimate concentrations)
- Use Real Gas equation of state for pressure above 100barg (Abel-Nobel EoS)

Pressure (barg)	$Z$
15.7	1.01
157	1.1
786	1.5

$$PV = ZRT$$

# Free under-expanded hydrogen jets

At least three reasons to study free under-expanded H<sub>2</sub> jets:

- They provide good, controlled data to validate the CFD tool
- The initial air entrainment is key to define the concentration profiles and is NOT affected by the ventilation (“momentum dominated region”)
- The jet generated shear turbulence is sufficient to produce strong overpressures upon ignition (differently from common HCs)

# Free hydrogen jets: Data

	P0 (barg)	T0 (degC)	D0 (m)	Release rate (kg/s)	z(m)	direction
Roberts &al., 2006	94	13	0.004	0.07	1.5	Horizontal
Daubech &al., 2015	40	10	0.012	0.25	1.5	Horizontal
Tanaka &al., 2007	400	10	0.008	1	1	Horizontal

Roberts & al., 0.07 kg/s



Daubech & al., 0.25 kg/s

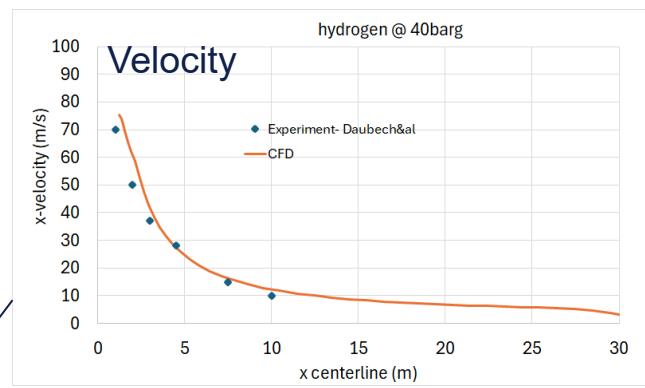
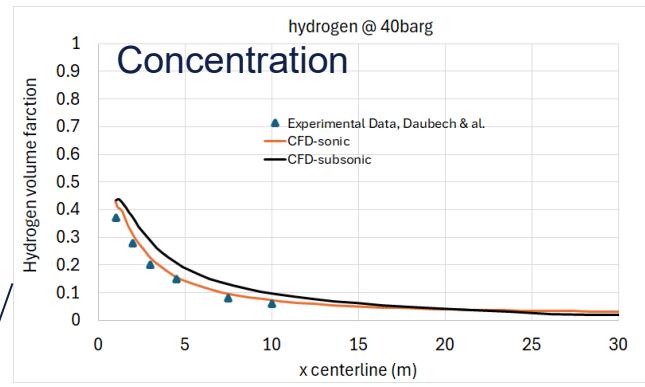
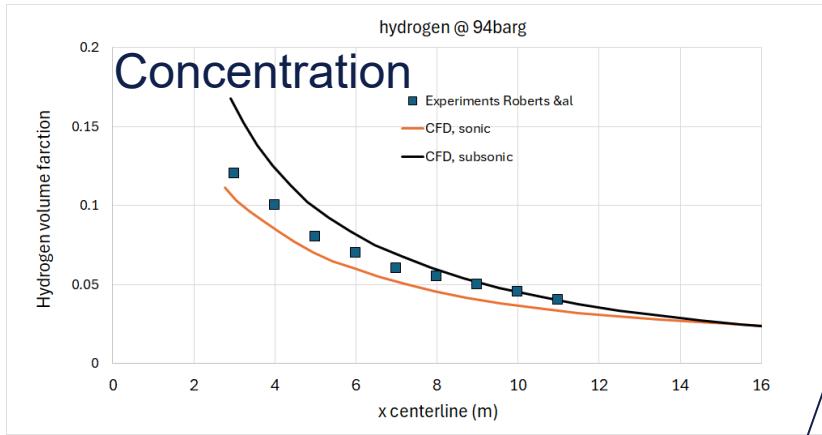


Tanaka & al., 1 kg/s

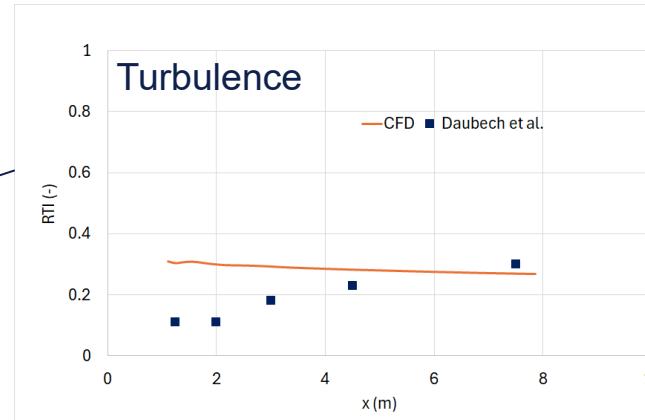


# Free hydrogen jets: Model Performance

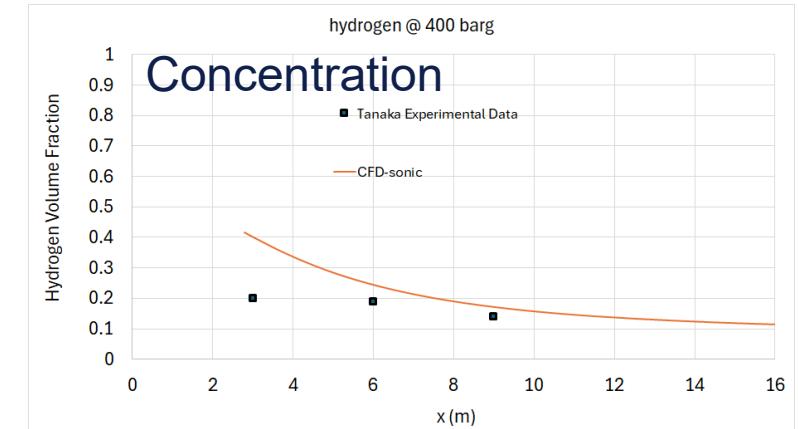
Roberts & al.



Daubech & al.



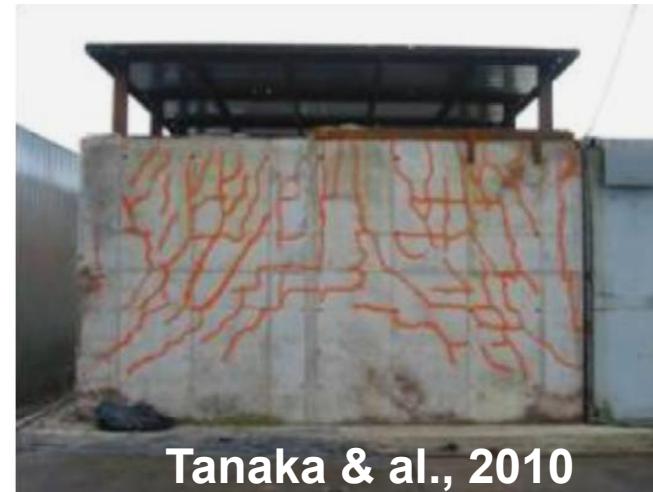
Tanaka & al.



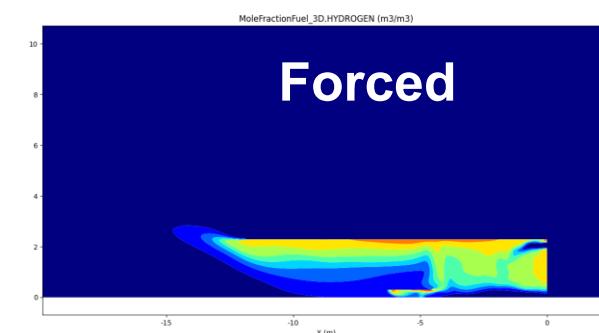
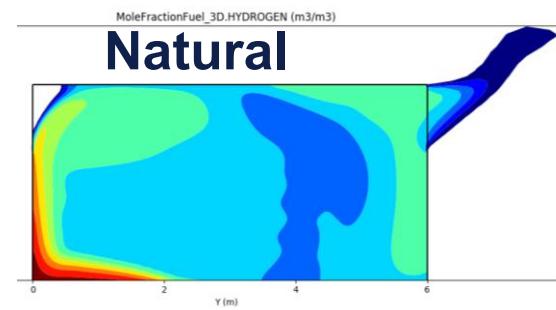
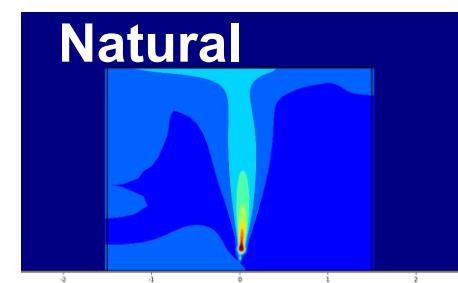
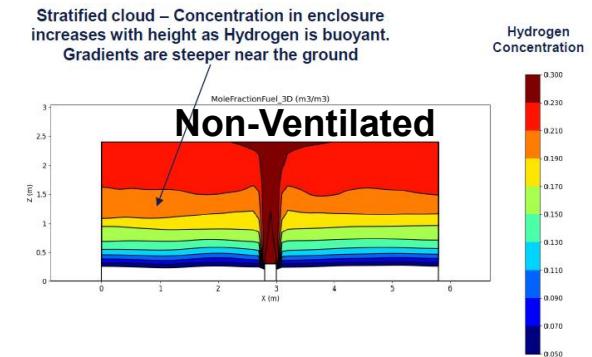
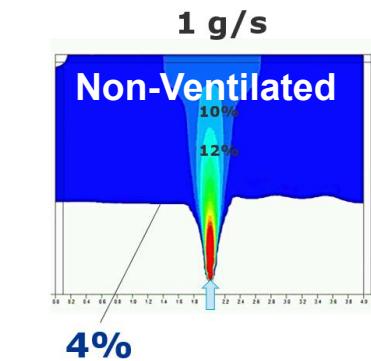
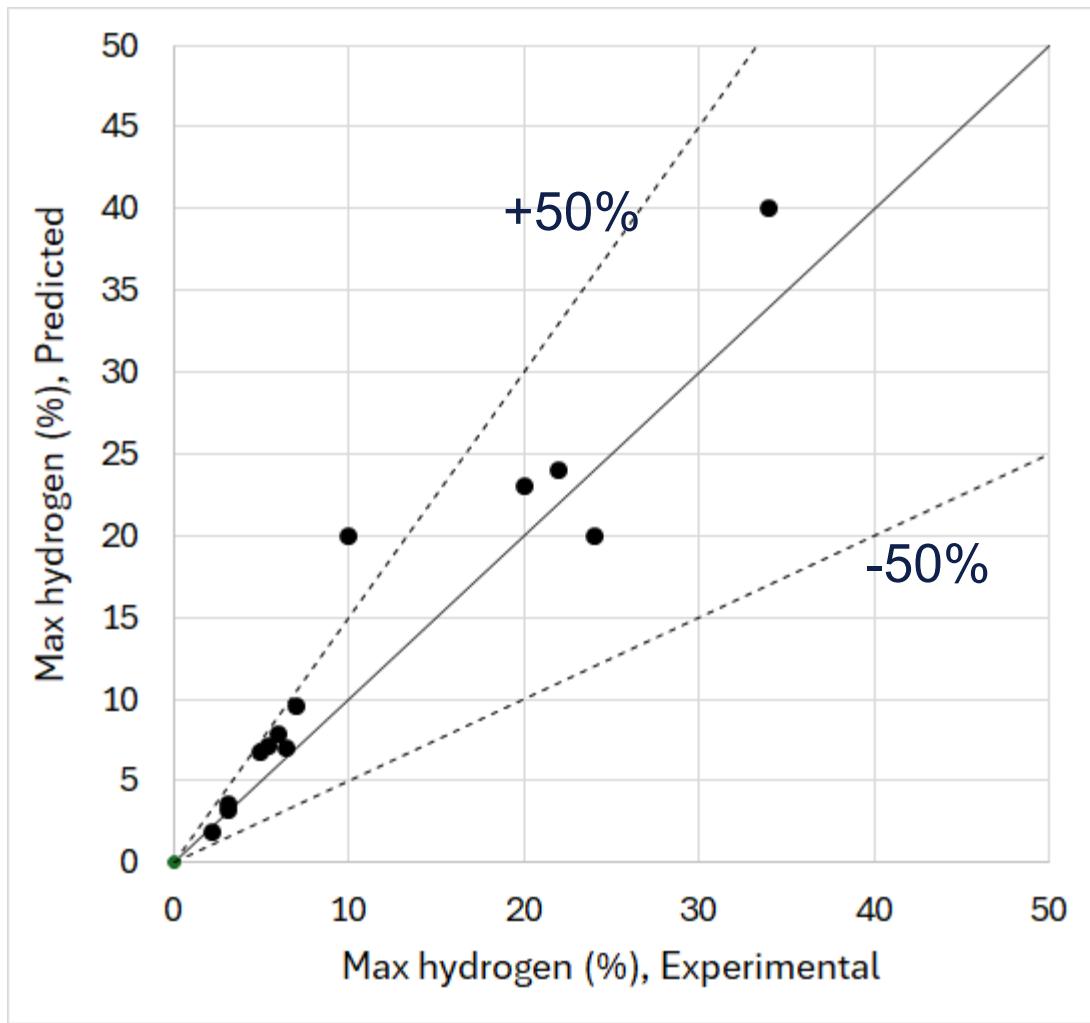
# Hydrogen Releases in Enclosures: Data

Test ID	Authors
1	Lacome & al., 2007-INERIS
2	Lacome & al., 2007-INERIS
3	Lucas & al., 2020- HySea
4	Lucas & al., 2020-HySea
5	Lowesmith & al., 2009- NaturalHy-DNV Spadeadam
6	Tanaka&al., 2010 - DNV Spadeadam
7	Tanaka&al., 2010 - DNV Spadeadam
8	Lach&al, 2021
9	Lach&al, 2021
10	Lach&al, 2021
11	Lach&al, 2021
12	Lach&al, 2021
13	Lach&al, 2021

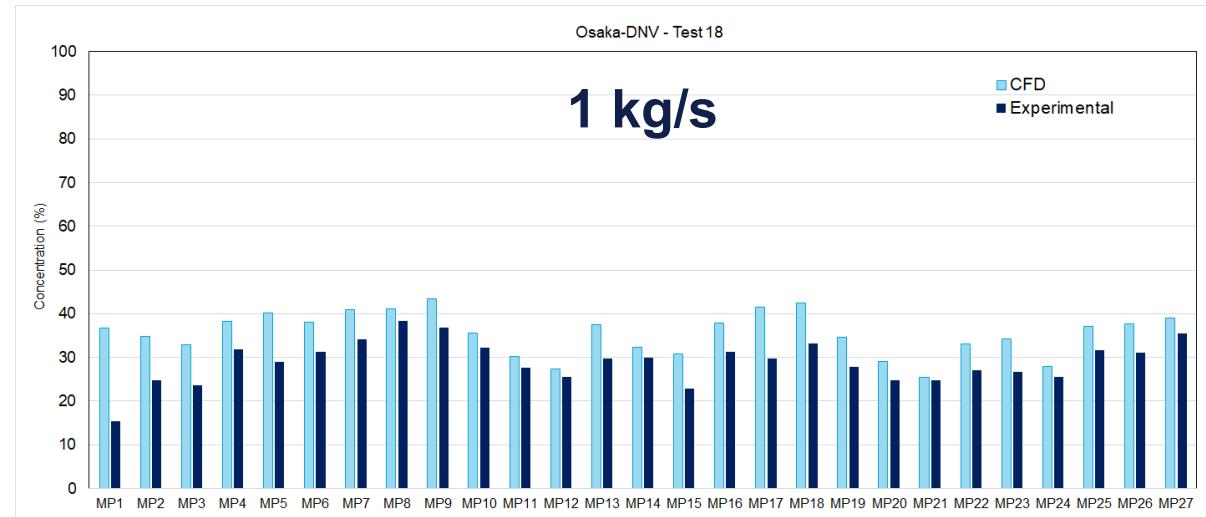
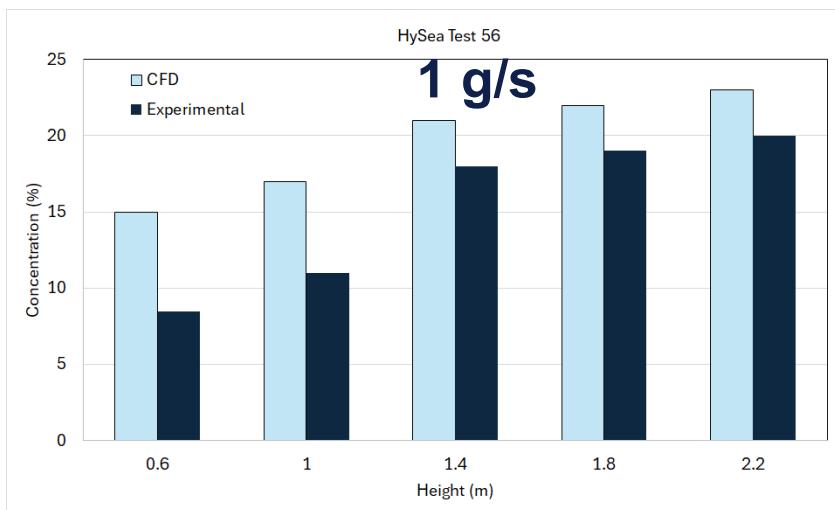
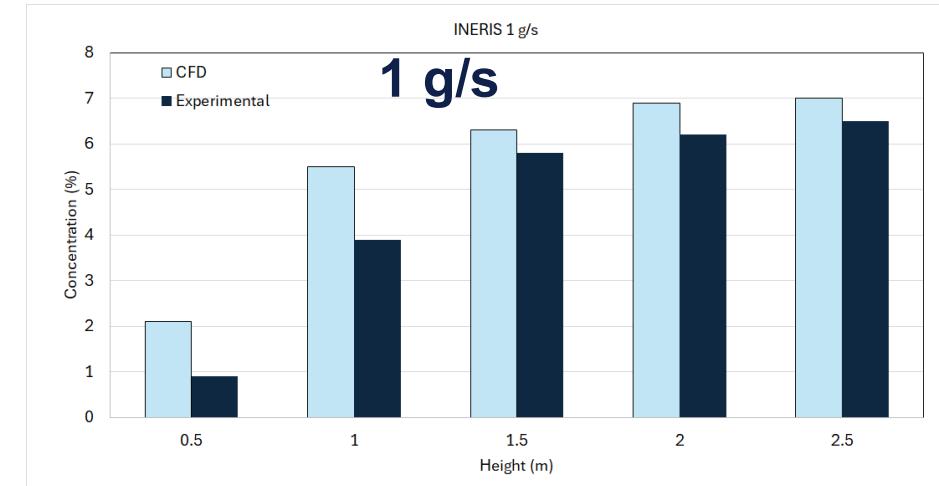
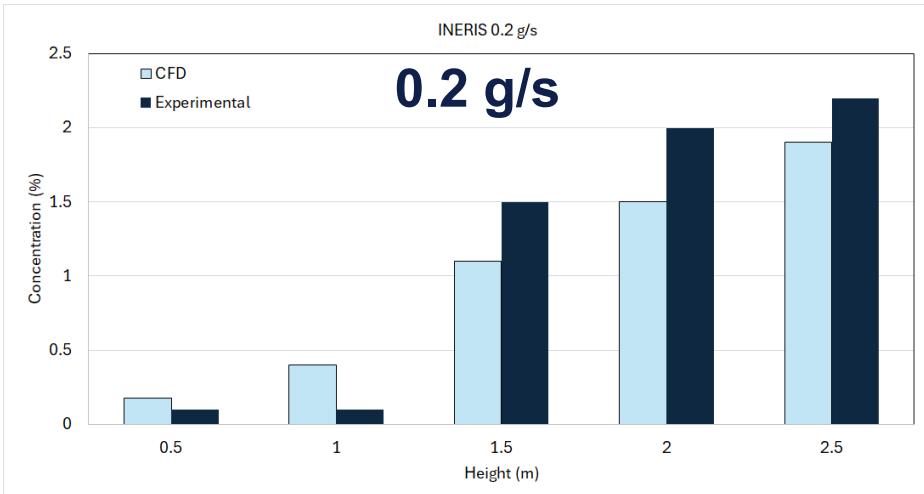
- Non-ventilated, natural and forced
- Pressure range: atm - 400 bar
- Release rates: 0.2 g/s – 1 kg/s
- Release: diffuse and jet
- Outflow velocities: subsonic and sonic
- Froude Number:  $10^2$  to  $10^7$



# Model Performance: Max Concentration



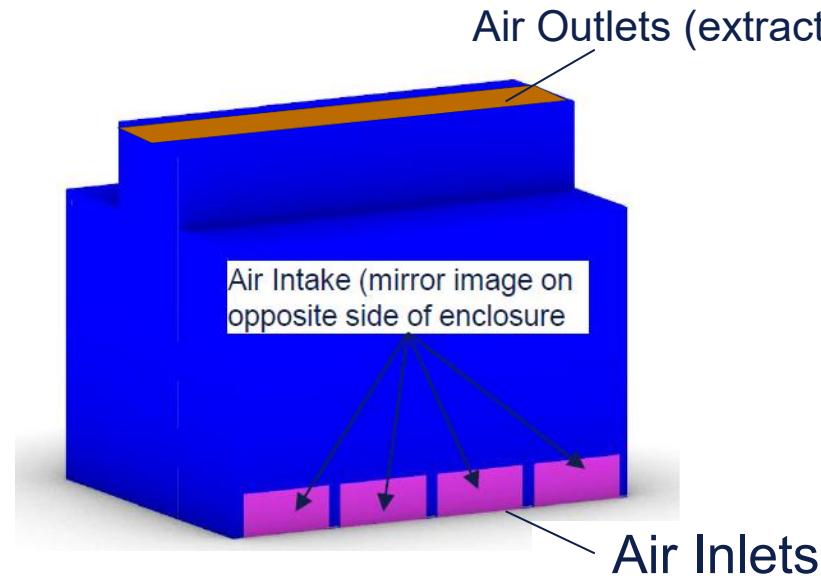
# Model Performance: Stratification



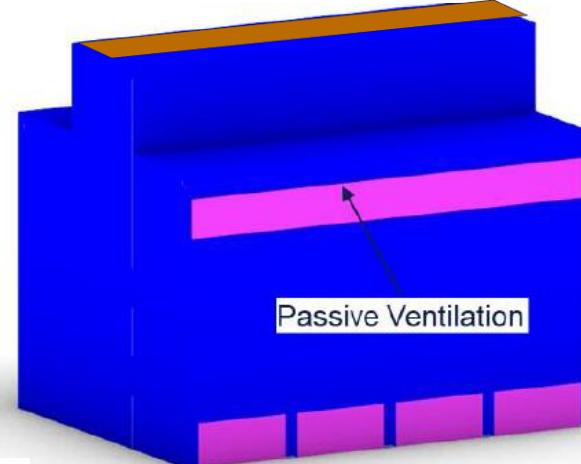
# Support to Design: Case Study

# Case Study: Configurations

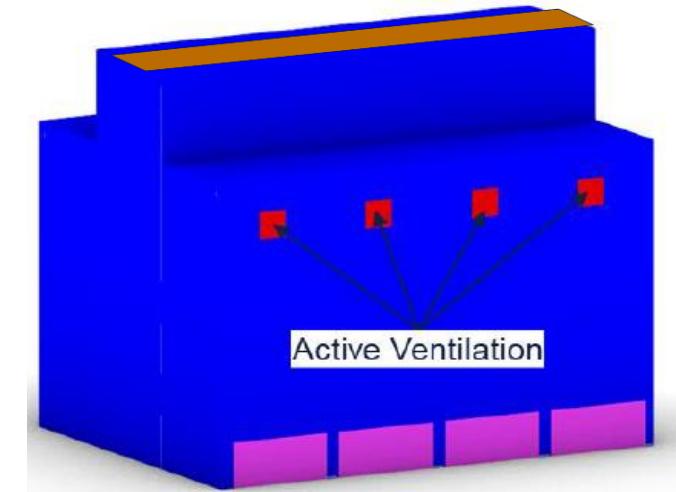
Five different ventilation configurations were studied with CFD for a compressor shelter (5,000 m<sup>3</sup>)



Air extracts at the roof;  
Air inlets at floor;  
**3** Ventilation Air Rates:  
50, 100, 200 kg/s  
(30, 60 and 120 ACH)

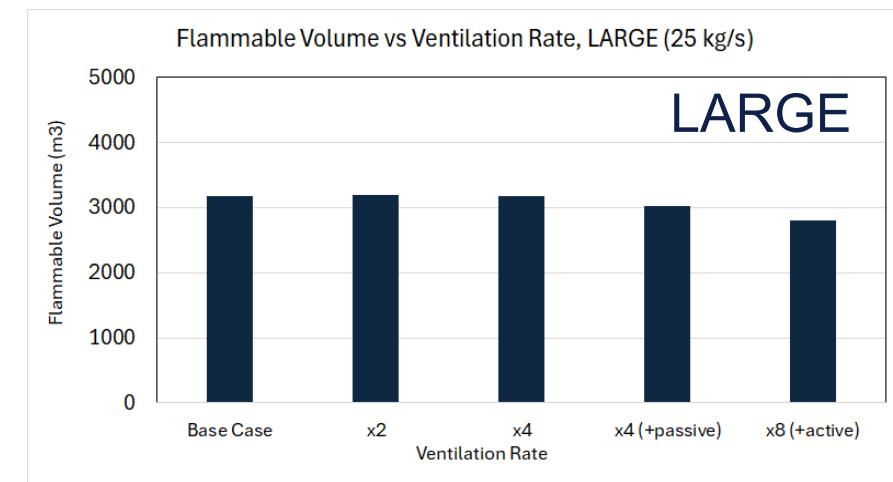
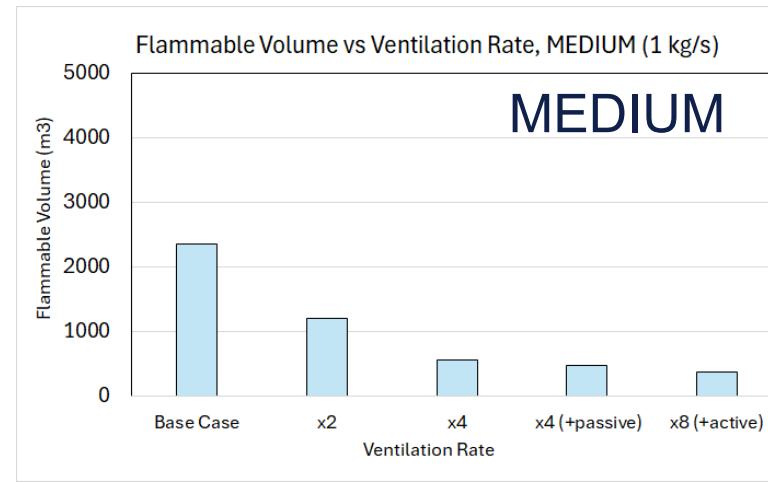
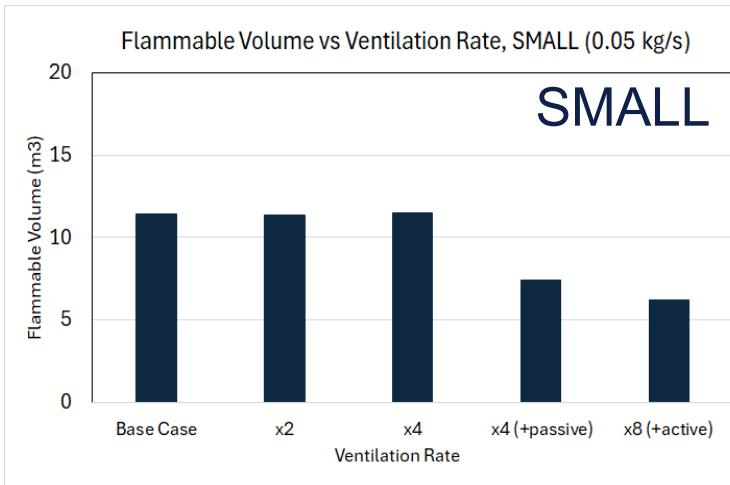


+ Side Wall Openings (passive)  
**1** Ventilation Air Rate: 200 kg/s  
(120 ACH)



+ Side Wall Openings (active)  
**1** Ventilation Air Rate: 400 kg/s  
(240 ACH)

# Case Study: Flammable Volume

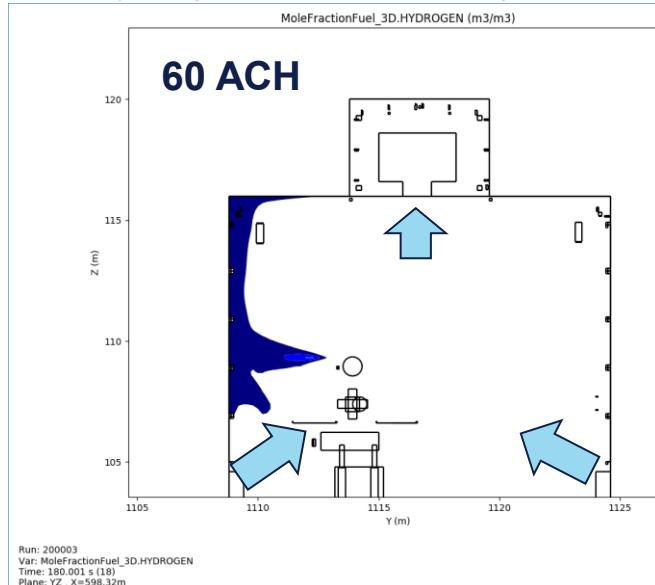


- Considerable reduction of flammable volume for the Small by adding side openings (50% reduction). In any case the Small releases generate filling fraction of order 0.1%
- Considerable reduction for the Medium by doubling the air ventilation rate (50% reduction). One order of magnitude reduction by an eightfold increase of the ventilation rate
- Modest reduction for the Large (even for an eightfold increase of air rate).
- Max filling fractions: 0.2%, 47% and 64% respectively for S, M and L
- Note that SMALL was calculated for 5mm; if 1 mm was considered,  $V_{f,max} = 1m^3 = 0.01\%$

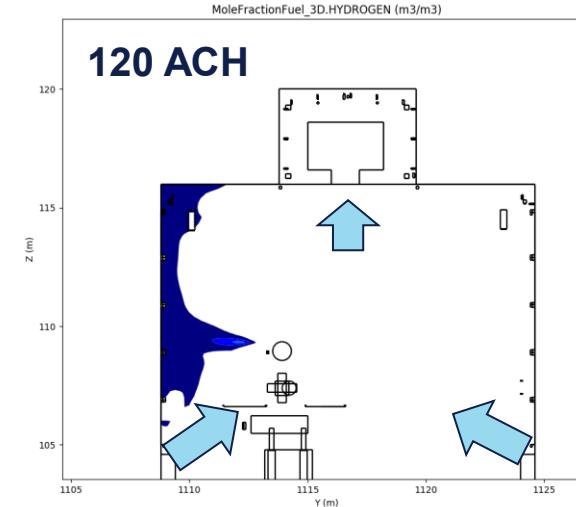
Configuration	ACH
Base Case	30
x2	60
x4	120
x8	240

# Case Study: Distribution of Inlets/Outlets

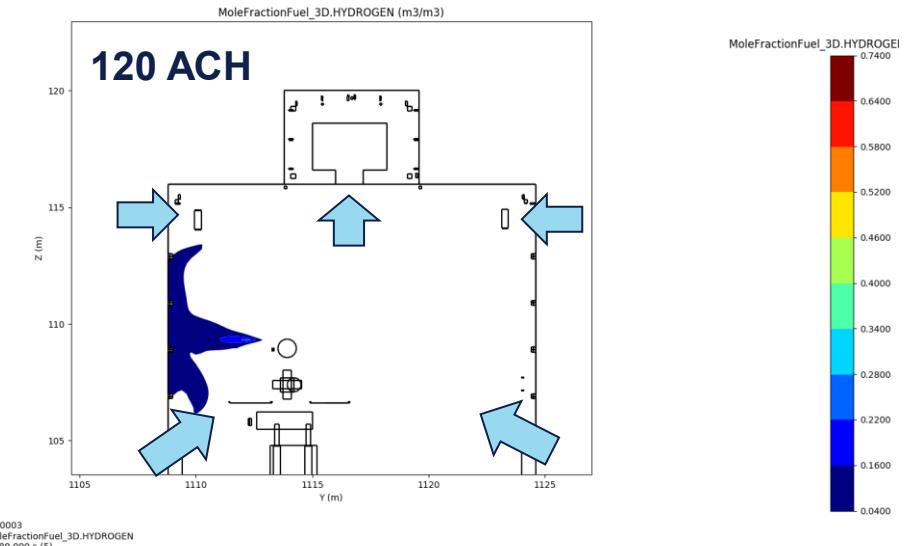
Hydrogen concentration (LFL-UFL)



Hydrogen concentration (LFL-UFL)



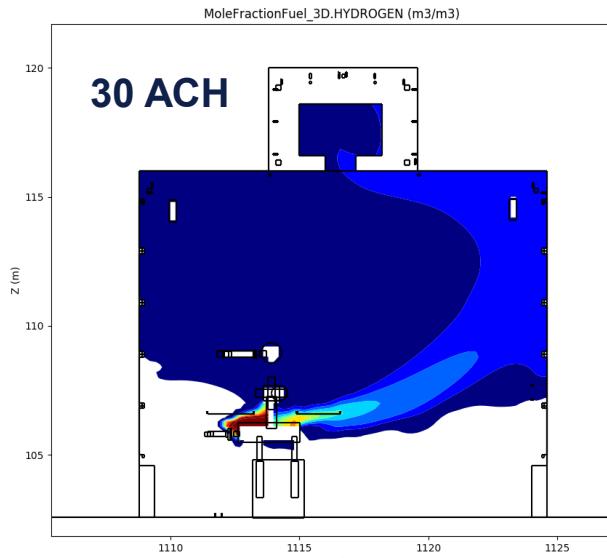
Hydrogen concentration (LFL-UFL)



- Side openings promote dilution of stagnant pockets
- In some conditions, ventilation rate alone is not enough, and distribution of inlets/outlets is more effective

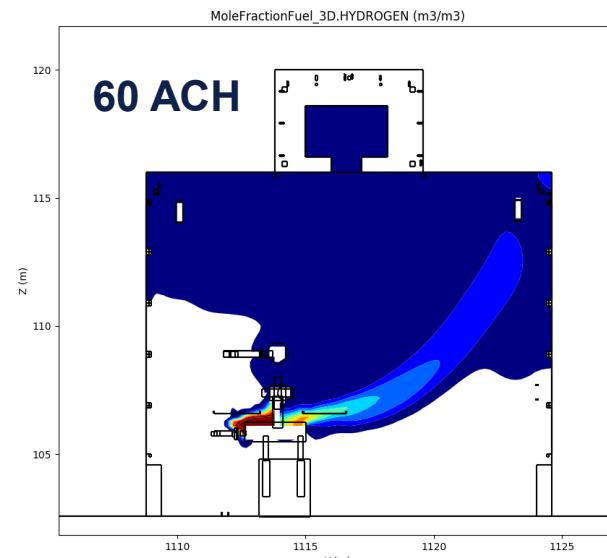
# Case Study: Increasing Air Rate

Hydrogen concentration (LFL-UFL)



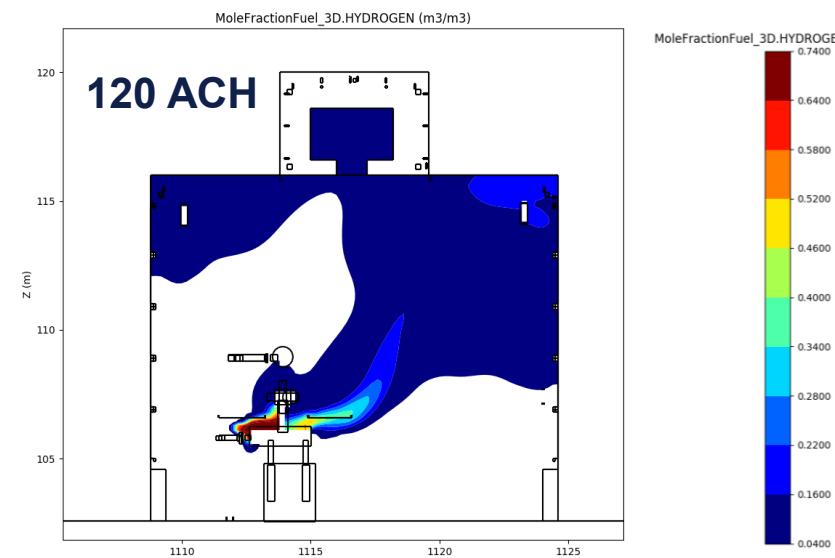
Hydrogen=1 kg/s

Hydrogen concentration (LFL-UFL)



Hydrogen=1 kg/s

Hydrogen concentration (LFL-UFL)



Hydrogen=1 kg/s

- Increasing air rate promote dilution of regions where gas has lost momentum and can clear significant part of the enclosure

# Support to Design: Remarks

- Ventilation has good potential to dilute flammable gas for S and M releases.
- The ventilation rate is not the only design parameter: distribution of air inlets and outlets is also key
- Even when dilution is good (S and M), ventilation alone cannot eliminate the flammable hazard (especially for high-pressure typical of a compressor room).
- It needs to be complemented with all the other mitigation measures: control of ignition sources, gas detection and automatic isolation, explosion relief venting, etc.
- Ventilation is not a substitute of good design (i.e., selection of material, minimization of the inventories, minimization of the size of the piping/connection etc.)

# Conclusions

# Conclusions

- Current guidance for the design of ventilation systems handling hydrogen is lacking or not fully quantitative
- CFD engineering tools can reproduce experimental trends - of systems handling hydrogen - in a wide range of conditions. Hence, they can be a valuable support for the design of ventilation
- A mix of modelling, full-scale testing - when possible - and a good look at the past is the best recipe to support design.

*“We see further by standing on the shoulders of giants”, Isaac Newton, 1675*

# Thank You

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[www.dnv.com](http://www.dnv.com)

# Geometry of the jet as a function of Froude Number

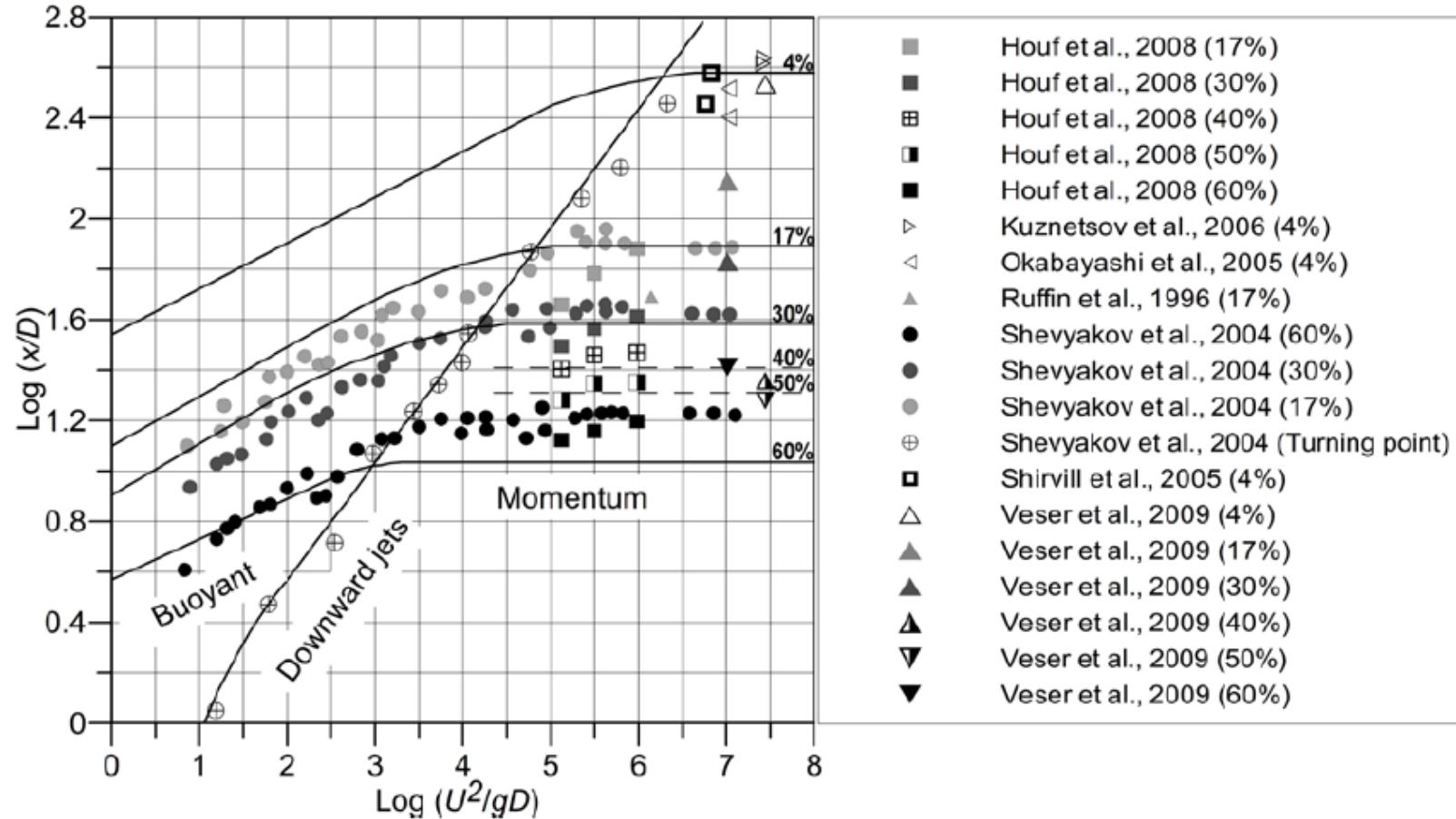
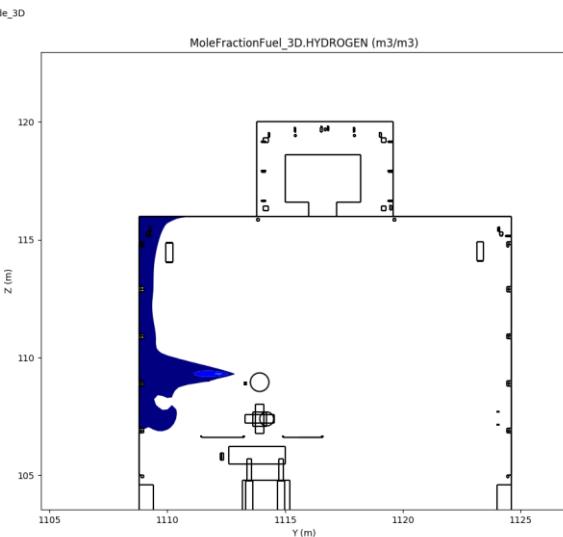
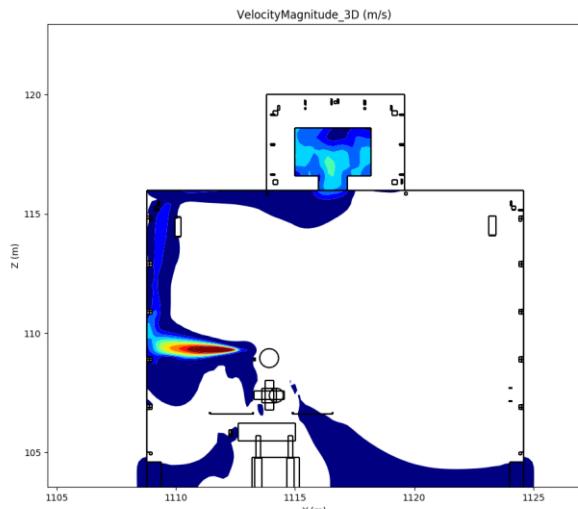


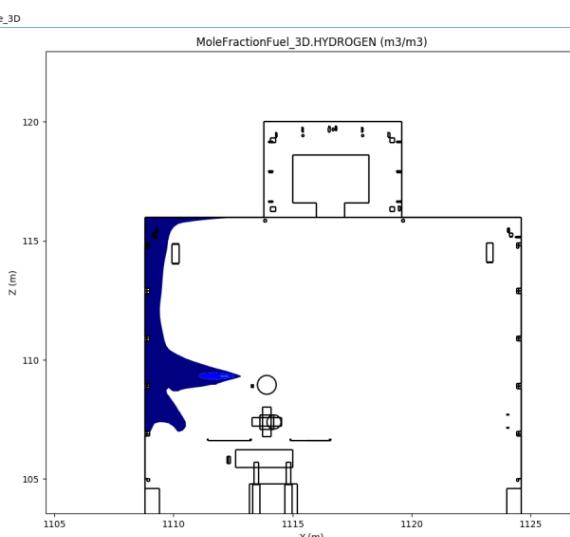
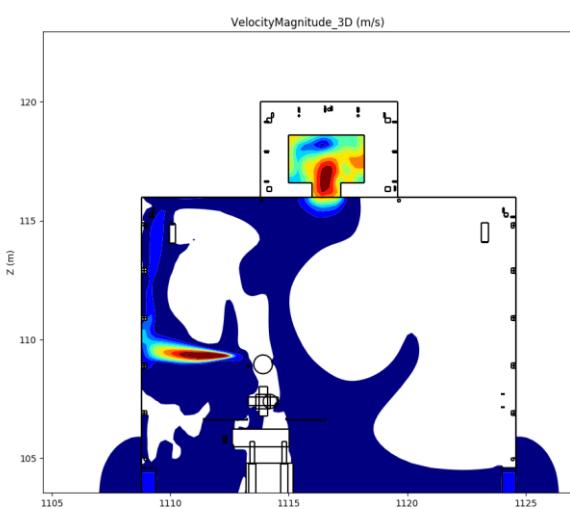
Figure 5-8. The dependence of the distance to nozzle diameter ratio for particular concentration of hydrogen in air on the Froude number.

# Small

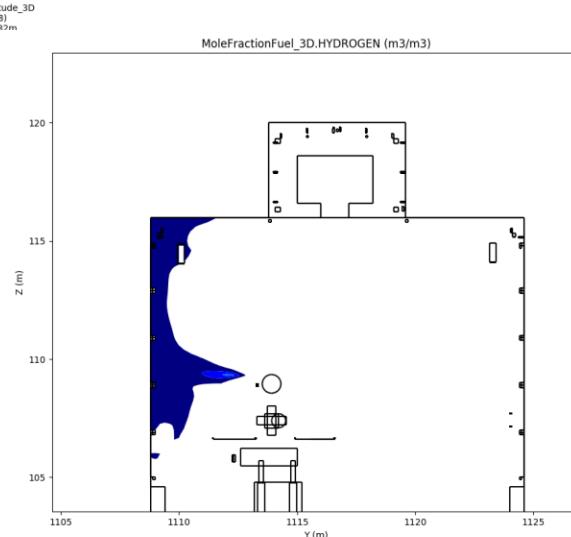
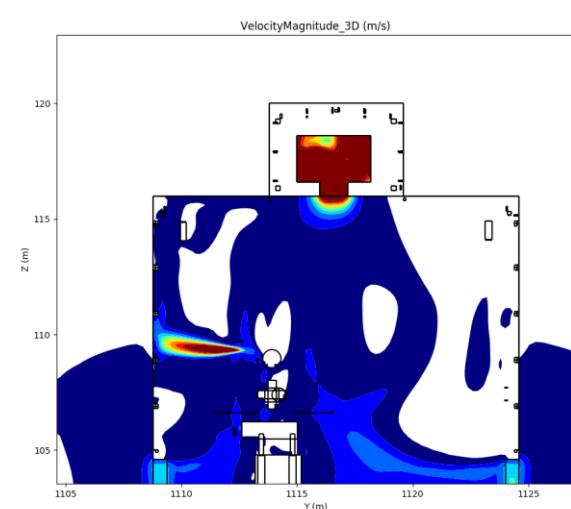
50 kg/s



100 kg/s



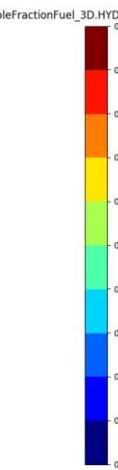
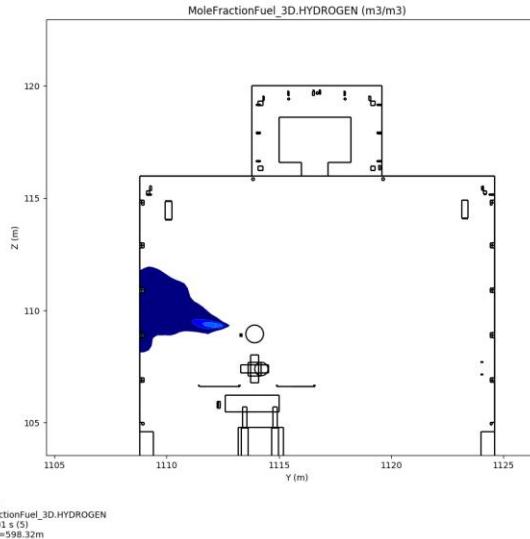
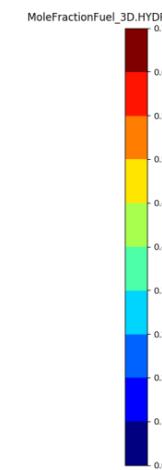
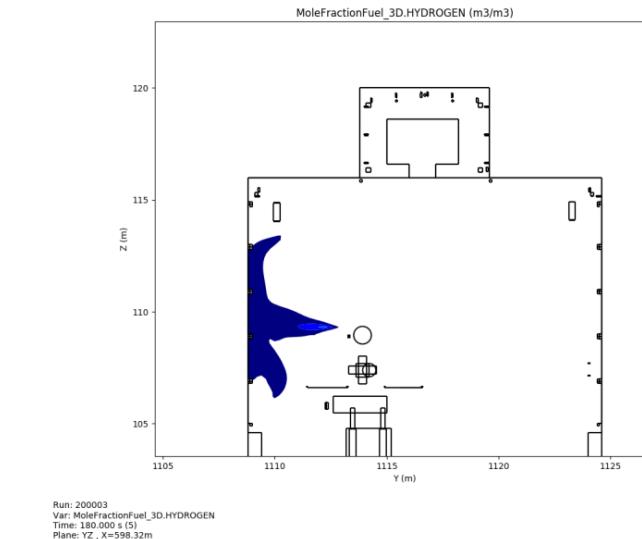
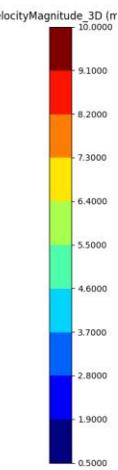
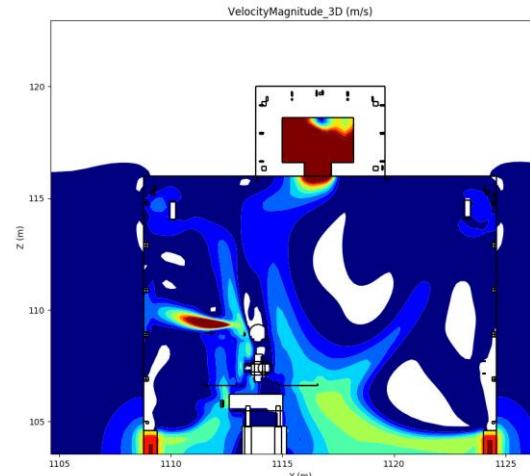
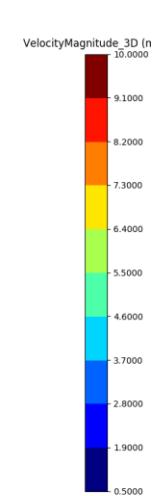
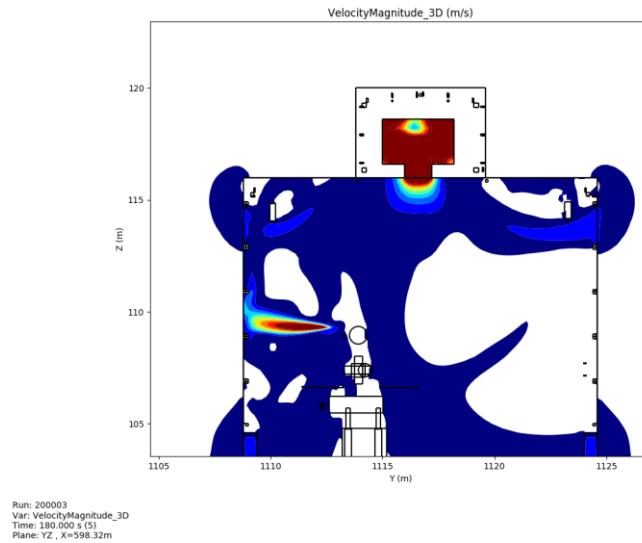
200 kg/s



# Small

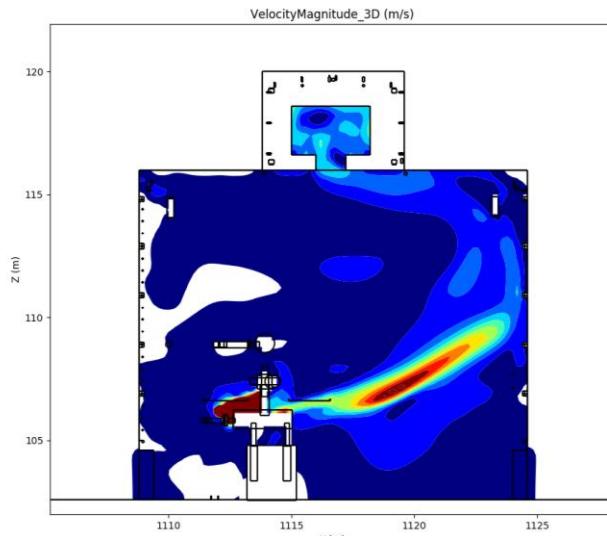
200 kg/s, additional side openings (passive)

400 kg/s, additional side openings (active, forcing air in)

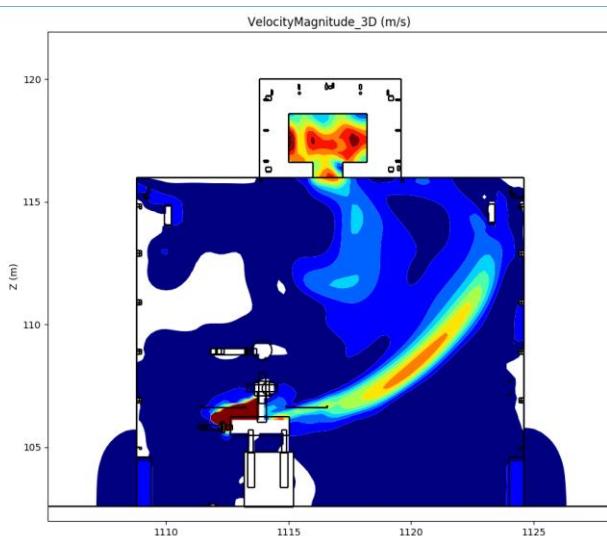


# Medium

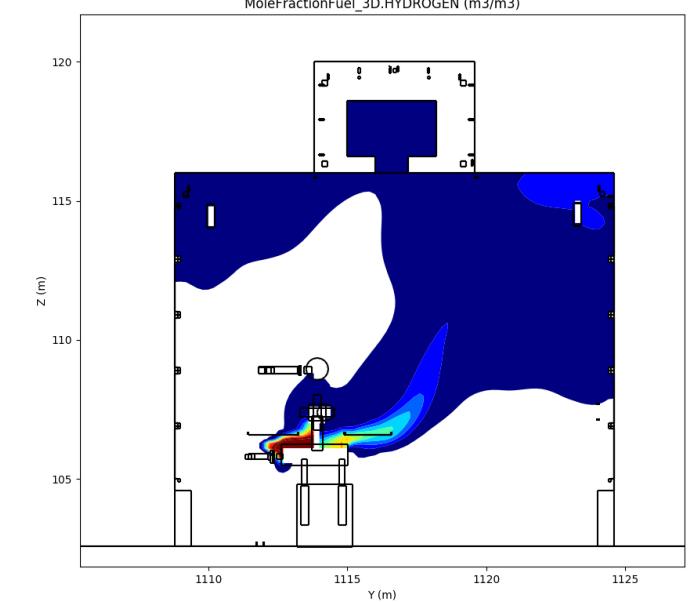
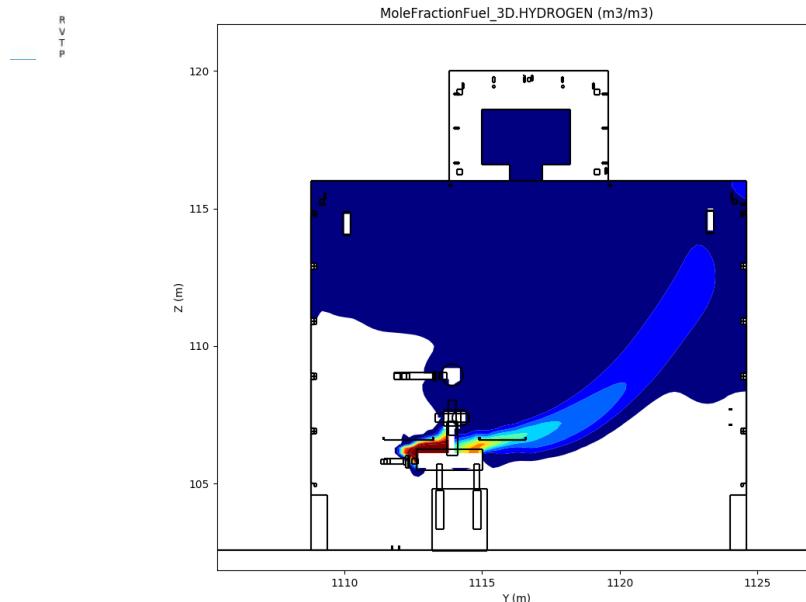
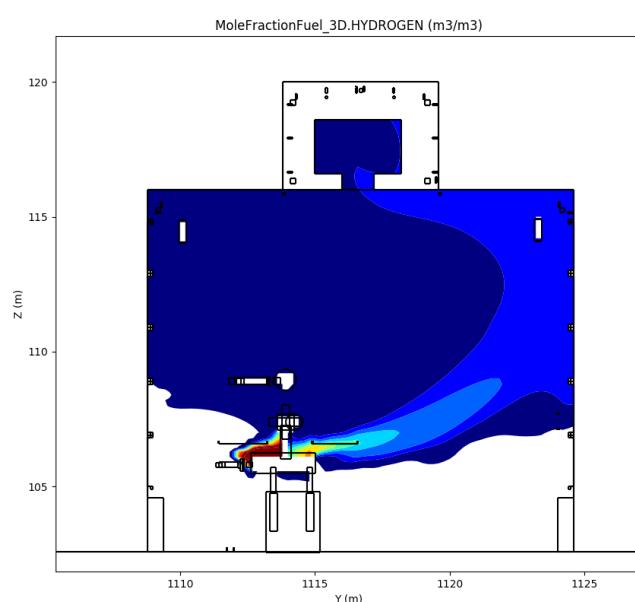
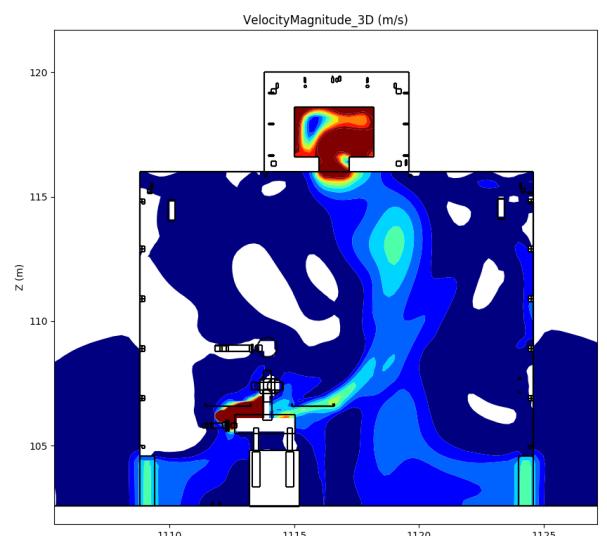
50 kg/s



100 kg/s

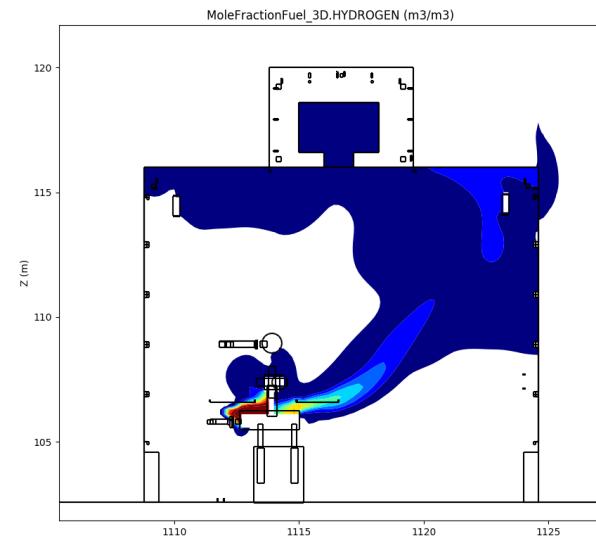
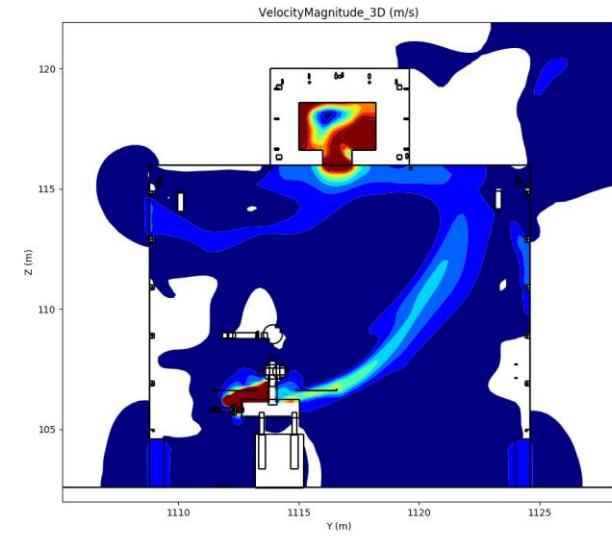


200 kg/s

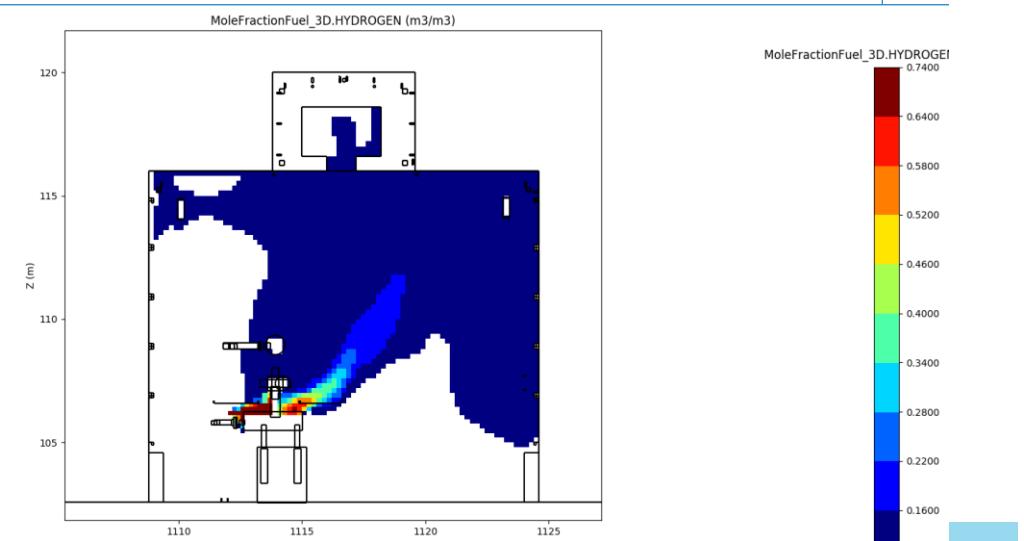
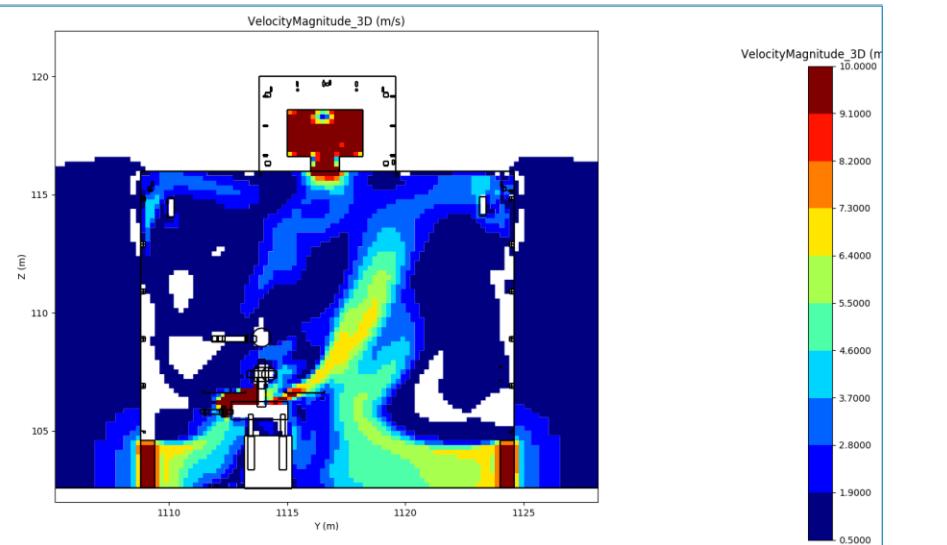


## Medium

200 kg/s, additional side openings (passive)



400 kg/s, additional side openings (active, forcing air in)



# Extraction Fans at the Roof

