# **Faculty of Engineering**



#### **Lean Premixed Turbulent Flames vs. Hydrogen Explosion: A Short Survey on Experimental, Theoretical and Analytical Studies**

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#### **Motivation**:

 **Safety considerations in hydrogen usage in general andcombustion in industrial applications**

#### **Study**:

 **Restricted to deflagration flames, with the emphasis on molecular effects (preferential diffusion and Lewis number)on lean premixed turbulent combustion: Pure Hydrogenflames and Hydrogen-Hydrocarbon flames**

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**: H2 influenced hydrocarbon flames**

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#### **Introduction**

**Experimental & theoretical convergence on lean hydrogenpremixed turbulent flames (spherical explosions)**

- **Backward-facing flame fronts are formed nearer the unburned than the burned side of the turbulent flame brush, suggesting the importance of large-scale flame-front bulges in turbulent flame propagation**
- **Superadiabaticy and flame-front bulges convex toward the reactants are clearly observed, representing effects of the lessthan-unity Lewis number of the mixture. The average size of flame bulges is found to increase with the turbulence integral length scale**

(Karpov,) Lipatnikov and Chomiak, Proc. Combust. Sym. Int. 1996, & Prog. in En. and Combust. Sci 2005

# **Flame Curvature, Mass Flow & Turbulent Flame Speed**



### **Preferential Diffusion and Lewis number Effects**



# **Lewis Number Effects – DNS investigations**

**<sup>❖</sup> DNS by Trouvé and Poinsot 1994 on lean H2/O2/N2 flames………………………………..**

 **and DNS of lean H2 flame by Bell et al. <sup>2006</sup> (not depicted here), confirm the Le influence on turbulent flame speed, especially in lean H2 mixtures**

**……………………………………………………**

 **This substantial rise in flame speed may be due to sum of DL and PDT effects, or, can also be explained using Leading Point concept**



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Trouve´ A, Poinsot T. Evolution equation for flame surface density in turbulent premixed combustion. JFluid Mech 1994;278:1–31.

## **Lewis Number Effects – Russian database**

 **Case1: For lean (**φ**=0.5, Le =0.45) H<sup>2</sup> mixture, SL0 is 5 times lower as compared with a rich (**φ**=2.0, Le=1.9)**  $H_2$ -air mixture, whereas the slope  $(S_T/u')$ shows the opposite behaviour and S<sub>T</sub> **is markedly higher for the former mixture at u'>1 m/s**

 **Case2: For very lean (**φ**=0.17, Le=0.4) H2 mixture (not depicted here), SL0 is by more than 15 times lower as compared with the above rich case, while ST for both cases are roughly equal**



# **Premixed Turbulent Combustion Model**

#### **Algebraic flame surface wrinkling premixed turbulent reactionsubmodel by Muppala, Aluri and Dinkelacker**





Muppala et al. Combust. and Flame 2005, & Prog. in CFD 2004

# **Leading Point Concept -- Critically Curved Flamelets**

**<sup>❖</sup> To predict the strong effect of Lewis number on turbulent flame<br>
creed exities!!\\eurved leminer flames have been prepased as a speed, critically curved laminar flames have been proposed as a model of the leading kernel structure by arguing that:** 

 **(1) the leading points should be associated with the highest local burning rate, and** 

 **(2) highest (for various possible perturbations of a laminar flame with Le<1) local burning rate is reached in such flames. The latter hypothesis has been substantiated by simulations of various perturbed laminar flames.**

 **Also, strongly curved, lean H2–air flames can survive under the influence of high strain rates. This behaviour is associated with the local increase in temperature in curved laminar flames, because the energy flux into the flame exceeds the heat losses from it if Le<1.**



III to Bradley's relation

### **2. Premixed Turbulent Combustion Model**

**Above relation failed to demonstrate the influence of hydrogen onhydrocarbons, and moreover, for very lean pure hydrogen flames**

**Modifications were carried out on algebraic flame surface wrinkling premixed turbulent reaction submodel using theconcept of Leading point related to critically curved flamelets**

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#### For Lewis numbers  $< 1$ , the flame ball temperature is given by  $T_r = T_u + (T_b - T_u)/Le$ 1.510exp $\dot{\phantom{1}}$  (2)  $T_{cr} = \tau_c \frac{R_{cr}}{\delta_{L0}} = \tau_c L e^{-1} \left( \frac{T_b}{T_r} \right) \exp \left( \frac{\Theta}{2T_b} \frac{T_b - T_r}{T_r} \right)$  $\tau_{cr} = \tau_c \frac{R_{cr}}{\delta_{L0}} = \tau_c Le^{-1} \left(\frac{T_b}{T_r}\right)^{1.5} \exp\left(\frac{\Theta}{2T_b} \frac{T_b - T_r}{T_r}\right) \longrightarrow \tau_{cr} = \tau_{c0} \frac{\left(u_c\right)_{t \to \infty}}{\max\left\{u_c(t)\right\}_{r = r_{cr}}}$ The chemical time scale for the highest local burning rate isThe mass flux of the deficient reactant throu' the surface of the flame ball scales as  $R_{cr}^{-1}$ **Critical chemical time scale = chemical time scale x consumptionrate (of undisturbed planar laminar flame)/maximum possible local consumption rate**(percepted at the convex part (positive curvature) of the flamelet facing towards unburned gas)**Leading Point Concept -- Critically Curved Flamelets**Aluri, **Muppala**, DinkelackerLipatnikov and Chomiak, 0.25  $\bigwedge$  0.2  $0.8 \quad 0.2$  $\overline{0}$  $0$  /  $\vee$   $P_0$ 0.46 $1 + \frac{3 \cdot 3}{2 \cdot 3 \cdot 4}$  $exp( Le - 1)$ *t* $T \sim L_0$ <sup>1</sup>  $\sigma$ <sub>1</sub>  $\sigma$ <sub>1</sub>  $\sigma$ <sub>1</sub>  $\sigma$ <sup>1</sup> $\sigma$ <sup>1</sup> $\sigma$ <sup>1</sup> $\sigma$ <sup>1</sup> *cp* $S_T = S_{L0} \left[ 1 + \frac{1}{\left(1 + \frac{1}{\$  $Le-1$   $\qquad \qquad$   $\qquad$   $\$ ττ $\left(1+\frac{0.46}{(1+\frac{0.46}{(1+\frac{0.8}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25}{(1+\frac{0.25$  $+$  $\left[1+\frac{0.40}{\exp(Le-1)}u^{\prime 0.8}s_{Lo}^{0.2}\left(\frac{\tau_t}{\tau_{c0}}\right) - \left(\frac{p}{p_0}\right) - \right]$  $\left[\begin{array}{cc} \exp(Le-1) & \stackrel{\scriptscriptstyle{L\omega}}{\sim} \left(\tau_{c0}\right) & \left(\begin{array}{c} p_0 \end{array}\right) \end{array}\right]$  $\frac{c_0 - \omega_l \omega_L}{L}$  $\overline{\tau_{c0}} = \alpha / S_{L0}$ Modified AFSW reaction model

Combust. and Flame 2006 Combust. Sci. and Tech. 1998

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0.5







# **Hydrogen Influenced Propane Flames –** Kido database





 $7,5$ 

 **Turbulent flame speed ST vs. u' for C3H<sup>8</sup> mixtures. Experiment vs. Model predictions (using S<sup>L</sup>, and in other two cases using SL0 but b) without, c) with Le term** 

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 $S_T/S_{10} - Exp$ 

5  $S_T/S_{LO} - Exp$ 

# **Summary on Hydrogen Explosion**

**❖ The hydrogen-hydrocarbon mixture is rendered less reactive for <br>
flame propagation with HC substitution flame propagation with HC substitution (Muppala et al 2006; Law and Kwon 2004; Kido et al 1998)**

 **Influence of hydrocarbon (e.g., propane) is realizable beyond 20% by vol. in mixtures of HC-H2 mixtures on turbulent flame speed (Muppala et al 2006; Halter et al 2006; Kido et al 1998)**

 **Experiments and analytical predictions showed that propane substitution to H2-air mixtures moderates cell formation due to PDT and Darrieus-Landau (hydrodynamic) instabilities (Law and Kwon 2004)**

 **There is potential of containing (or at least retarding) the occurrence of DDT in confined structures with addition of hydrocarbons to hydrogen mixtures(Abdel Aal 2005; Law and Kwon 2004)**

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